

Homework 3.

3-1 $C_{Fe^{2+}} = 13 \text{ g/m}^3$



55.8 g/mol 4e⁻

$$\therefore C_{O_2} = \frac{13}{55.8} \times \frac{1}{4} \times 32 \approx 1.86 \text{ g/m}^3$$

normally loaded urban wastewater BOD₅ ~~150~~ ¹⁷⁰ g/m³.

$$\frac{1.86}{150} \approx 0.7\%$$

$$\frac{1.86}{170} \approx 1.09\%$$

slides - 01 P 30
typical concentration.

3-2 a) $C_{eff-P} = 0.5 \text{ g/m}^3$ $Fe/P = 2.0$ _{1.8}

$C_{in-P} = 6 \text{ g/m}^3$

$Q = 25000 \times 0.45 = 12500 \text{ m}^3/\text{d}$

$M_{FeCl_3} = 55.8 + 2 \times 35.5 \times 3 = 162.3 \text{ g/mol}$

$m_{FeCl_3} = \frac{6}{31} \times 2 \times 162.3 = 62.8 \text{ g/m}^3$
_{1.8} $\times 12500 \text{ m}^3/\text{d}$

\checkmark
~~m~~ $40\% FeCl_3 = \frac{0.77}{0.4} = 1.92 \text{ t/d}$ _{m³} $= 0.77 \text{ t/d}$ $0.6P \text{ t/d}$
 $1.75 \text{ m}^3/\text{d}$

Price = $0.77 \times 250 = 192.5 \text{ CHF/d}$ 173 CHF/d

b) $C_{O,P} = 6 \text{ g/m}^3$ $C_{O,BOD} = 130 \text{ g BOD/m}^3$ $X_{0,55} = 100 \text{ g/m}^3$

$$SP_{C,p} = 6.8 \times \frac{C_{o,p}}{C_{o,BOD}} = 6.8 \times \frac{6}{130} = 0.31 \text{ kgSS/kg BOD}$$

$$SP_p = SP_{C,p} Q_o C_{o,BOD} \\ = 0.31 \times 12150 \times 130 \approx 500 \text{ kgSS/d}$$

$$\theta_x = 5d, \quad T = 10^\circ\text{C}, \quad F_T = 1.072^{(T-15)} = 0.706$$

$$SP_{C,BOD} = 0.75 + a b \times \frac{X_{o,SS}}{C_{o,BOD}} - \frac{0.102 \cdot \theta_x \cdot t_T}{1 + 0.17 \cdot \theta_x \cdot F_T} \\ = 0.75 + 0.6 \times \frac{100}{130} - \frac{0.102 \times 5 \times 0.706}{1 + 0.17 \times 5 \times 0.706} \\ = 0.75 + 0.46 - 0.225$$

$$\approx 0.9865 \text{ kgSS/kg BOD}_5$$

$$T = 12^\circ\text{C}, \quad F_T = 1.072^{-3} = 0.81$$

$$SP_{C,BOD} = 0.75 + 0.46 - \frac{0.102 \times 5 \times 0.81}{1 + 0.17 \times 5 \times 0.81}$$

$$= 0.965 \text{ kgSS/kg BOD}_5$$

$$\frac{SP_{C,p}}{SP_{C,BOD}} \Rightarrow 31.4\% \sim 32.1\%$$

$$X_{o,SS} = 0.5 \cdot T_{SS} \quad ???$$

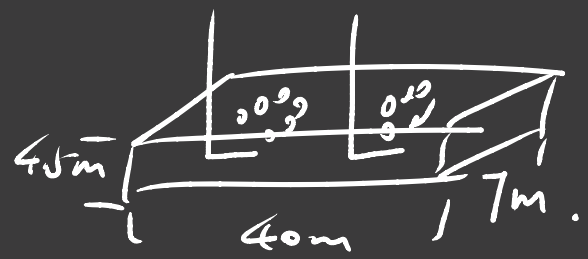
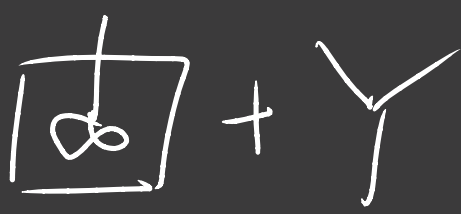
$$C_{o,BOD} = 0.75 \cdot S_{BOD_5}$$

after primary treatment

$$BOD_5 \Rightarrow 75\%$$

$$T_{SS} \Rightarrow 50\%$$

3-3

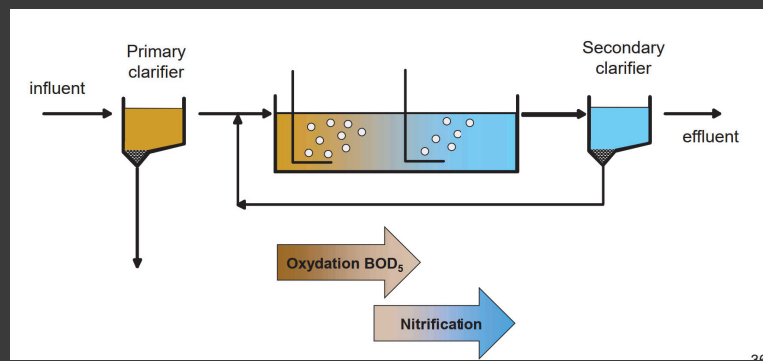


$N_{TKN} - N_{eff} = 2 \text{ g}_N/\text{m}^3$ $\times 3$ $V = 1260 \text{ m}^3$

$Q_0 = 10000 \text{ m}^3/\text{d}$ $S_{BOD_5} = 190 \text{ g}/\text{m}^3$ $TSS_{int} = 170 \text{ g}_{TSS}/\text{m}^3$

$N_{TKN, int} = 54 \text{ g}_N/\text{m}^3$ $N_{TKN} - N_{int} = 36 \text{ g}_N/\text{m}^3$

a). nitrification required. should not be completely mixed.



plug flow.

b) $V = 1260 \times 3 = 3780 \text{ m}^3$ $T = 10^\circ\text{C}$ $\theta_x = 10\text{d}$

$C_{0, BOD} = 0.75 \times S_{BOD_5} = 142.5 \text{ g}/\text{m}^3$

$X_{0, SS} = 0.5 \times TSS_{int} = 85 \text{ g}/\text{m}^3$

$F_T = 0.706$ X_{AT} with nitrification $2.5 - 3.5 \text{ kg}_{SS}/\text{m}^3$

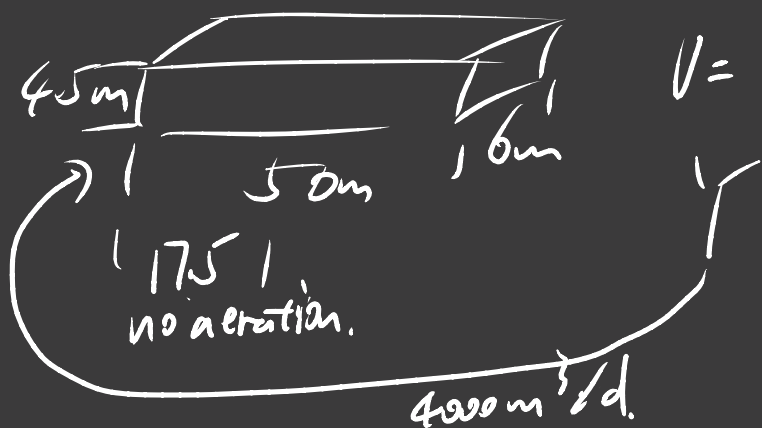
$$SP_{C, BOD} = 0.75 + 0.6 \times \frac{85}{142.5} - \frac{0.102 \times 10 \times 0.706}{1 + 0.117 \times 10 \times 0.706}$$

$$= 0.78 \text{ kg}_{SS} / \text{kg}_{BOD}$$

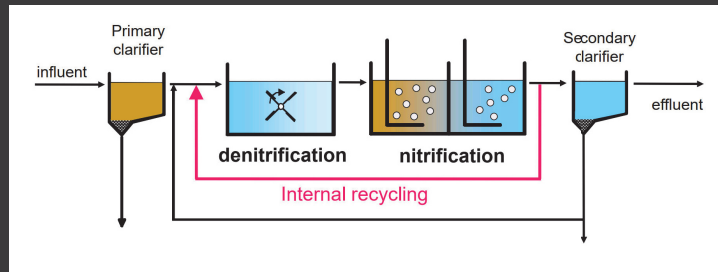
$$V_{AT} = \frac{Q_0 \cdot C_{0, BOD} \cdot SP_{C, BOD} \cdot \theta_x}{X_{AT}}$$

$$= \frac{10000 \times 0.1425 \times 0.78 \times 10}{3} = 3705 \text{ m}^3 < 3780 \text{ m}^3$$

3-4 $Q_0 = 5000 \text{ m}^3/\text{d}$ $S_{BOD5} = 260 \text{ g/m}^3$ $TSS_{\text{inf}} = 195 \text{ g TSS/m}^3$
 $N_{TKN-\text{inf}} = 63 \text{ g N/m}^3$ $N_3 - N_{\text{eff}} = 25 \text{ g N/m}^3$ $N_{TKN-\text{eff}} = 2 \text{ g N/m}^3$



$V = 50 \times 6 \times 4.5 \times 3 = 4050 \text{ m}^3$



pre-denitrification, N removal less.

$C_{0, BOD} = 0.75 \times BOD_5 = 0.195 \text{ kg/m}^3$

$X_{0, SS} = 0.5 \times TSS_{\text{inf}} = 0.0975 \text{ kg/m}^3$

10% TKN loss after primary treatment.

$\Delta N = 0.1 \times 63 - 25 - 2 - 0.045 \times 195 = 20.175 \text{ g/m}^3$

$r_{\text{den}} = \frac{\Delta N}{C_{0, BOD}} = \frac{20.175}{195} = 0.103 \text{ kg N-NH}_3 / \text{kg BOD}_5$
 ≈ 0.11

$\therefore V_D / V_{AT} = 0.2$

now $V_D / V_{AT} = 17.5 / 50 = 0.35 >> 0.2$

$R_x = 12.5 \text{ d}$

$SP_{C, BOD} = 0.75 + 0.6 \times \frac{195}{195} - \frac{0.102 \times 12.5 \times 0.706}{1 + 0.17 \times 12.5 \times 0.706}$

$= 0.69 \text{ kg SS / kg BOD}_5$

if $X_{AT} = 2.5 \text{ kg TSS/m}^3$.

$$V_{AT} = \frac{Q_0 \cdot C_{O,BOD} \cdot SPC_{BOD} \cdot \theta_x}{X_{AT}}$$

$$= \frac{5000 \times 0.175 \times 0.67 \times 12.5}{2.5} = 3363.75 \text{ m}^3.$$

$$V_{AT}/3 = 1121.25 \text{ m}^3 < V_{AT}' = 4050/3 = 1350 \text{ m}^3$$

$$V_D = 0.2 V_{AT} = 224.25 \text{ m}^3 < V_D' = 1350 \times 0.35 = 4725 \text{ m}^3$$

η_N .

$$\Delta N_D = 20.725 \text{ g/m}^3$$

$$\Delta N_N = 0.7 \times 63 - 2 - 0.045 \times 175 = 45.725 \text{ g/m}^3$$

$$\eta_N = \frac{\Delta N_D}{\Delta N_N} = \frac{20.725}{45.725} = 0.456$$

$$r = \frac{1}{(1 - \eta_n)} - 1 = 0.867$$

$$+ 0.5 = 1.367.$$

re circulation rate \downarrow .

pH. / alkalinity.